

STRETCH WRAP FILM

Stretch wrap films are used extensively in packaging to package discrete units together to form a unitary package and are also frequently used to attach a package to a palette, for example. Stretch wrap film may also be used as wrapping to protect a commodity from the environment during handling and transport.

Stretch wrap may be applied by an automatic or semi-automatic machine which includes stretch rollers to pre-stretch the film before it is wrapped around a package. Alternatively the stretch wrap may be applied manually by applying the film from a roll supported on a simple hand-held mandrel. The present application has particular application to this latter category of stretch wrap material, and also to film for use on machines in which the amount of stretch prior to wrapping is low or zero.

EP-A-0531021 describes a process for producing a stretch wrap plastic film in which the film is "cold stretched" at ambient temperatures to thereby plastically and elastically stretch the film to cold orient it. The cold oriented film is then allowed to relax to recover substantially its elastic deformation before being formed into a roll. This arrangement provides a film wrap which is substantially as economical, and may be more economical, in film usage when applied by a hand wrapping device than other stretch wrapping films are when applied by automatic and semi-automatic machinery including power pre-stretching devices. The process described in this patent specification has been commercially successful but, in practice, it has not been possible to achieve consistently as high a stretch ratio as 1:4 suggested in the patent specification without experiencing difficulties due to film breakage.

According to this invention a method of making a plastics stretch film comprises the steps of taking a cast or blown film of LLDPE at a temperature of between 50°C and 100°C, stretching it in two successive stretching steps,

the first step having a stretch ratio higher than that of the second step, to cause both plastic and elastic deformation of the film, relaxing the stretched film substantially to release all of the elastic deformation and  
5 winding the substantially relaxed film into rolls.

Preferably, stretching is performed at a temperature of between 75°C and 90°C.

By having a film in the temperature range specified above and stretching it in two successive stages it has  
10 been found that it is possible to produce more consistently a pre-stretched film. The film also has advantages in having a clearer, less opaque appearance.

Preferably the stretching of the film that occurs in the two successive steps has a stretch ratio in a range  
15 from 1:1.5 to 1:2.5 for each step. More preferably, the first stretch ratio is in the range 1:1.85 to 1:1.95 and the second stretch ratio is in the range 1:1.70 to 1:1.80. Preferably during the relaxing step there is a reduction ratio of substantially 1:0.85 between the speed of the film  
20 during the second stretch rolling step and the speed of the film during wind-up.

Preferably the temperature of the stretch film is substantially 80°C during the stretching steps. The plastics film may be at this temperature by carrying out  
25 the stretching steps at an appropriate position downstream of a casting or blowing/extrusion production line so that the method in accordance with the present invention is carried out in line with the film production. Preferably however the method of the present invention is carried out  
30 out of line with the basic film production process and, in this case, the film is preferably re-heated, for example by being passed over one or more heated rollers immediately before the stretching steps.

The plastics material particularly preferred for the  
35 stretch film of the present invention is linear low density polyethylene (LLDPE). This material is a copolymer of ethylene with a C<sub>4</sub> to C<sub>10</sub> olefin; for example, butene-1, 3-

methy1-butene-1, hexene-1, 3-methyl-pentene-1, 4-methylpentene-1, 3-methyl-hexene-1, octene-1, decene-1 or a mixture thereof. The alpha-olefin is usually present in an amount from 1 to 10 weight percent of the copolymer. A  
5 typical manufacturing process for the formation thereof is disclosed in US-A-4076698 and 4205021. The preferred LLDPE has a density ranging from 0.900 to 0.940 g/cm<sup>3</sup>. This material preferably has a melt index of from 1 to 6. A multilayer film is also suitable, such as a multilayer film  
10 having a three layer A-B-C structure wherein the A layer comprises LVLDPPE, the B layer comprises metallocene LLDPE and the C layer comprises LMDPE.

A particular example of a process in accordance with this invention will now be described with reference to the  
15 accompanying drawing which is a diagrammatic illustration of the process.

A plastics stretch film of 17, 20 or 23  $\mu$ m thick material consisting of 100% LLDPE sold under the trade description 17, 20 or 23 UP 050 by Mima Films s.c.a. of 148  
20 Route d'Arlon, L-8010 Strassen, Luxembourg is taken from a feed roll 1 through a nip formed between a first heater roller 2 and an idle roller 3. The film then passes around the top of heater roller 2 around the bottom of a heater roller 4 and around the top of a heater roller 5. All  
25 three heater rolls 2, 4 and 5 are provided with a recirculating supply of oil heated to 80°C. Heater rollers 4 and 5 are driven in opposite senses at a peripheral speed of 65 metres per minute. The heater roller 2 idles. As the film passes over the heater rollers 2, 4, and 5 it is  
30 heated to a temperature of 80°C. The heater rollers are formed from a material having a high heat conductivity. Chrome rollers have been found to be particularly effective.

The heated film then passes beneath a first rubber  
35 covered stretch roller 6 which has a peripheral speed of 66 metres per minute. A second rubber covered stretch roller 7 is located very close to stretch roller 6, 1 mm or less,

and is driven in the opposite sense to the first stretch roller 6 at a peripheral speed of 126 metres per minute. This stretches the film with a stretch ratio of 1:1.91, or 91% stretch. A third stretch roller 8 which is again  
5 located physically close to stretch roller 7 at a spacing of 1 mm or less is driven in the same sense as the first stretch roller 6 at a peripheral speed of 217 metres per minute. This stretches the film with a further stretch ratio of 1:1.72 or 72% stretch. An idler roller 9 creates  
10 a nip with the third stretch roller 8 to prevent slippage of the plastics film. As the film passes between the stretch rollers 6 and 7 and stretch rollers 7 and 8 it is stretched in two steps with a total stretch ratio of 1:3.3 or a stretch of 230%. The close proximity of the stretch  
15 rollers 6 and 7 and 7 and 8 prevent substantial necking-down of the plastics film material during its stretching.

The film leaving the nip between the third stretch roller 8 and the idler roller 9 then passes over a third idler roller 10 before passing around the surface of a  
20 polished roller 11 which has a peripheral surface moving in the opposite direction to the direction of movement of the film, before being wound on a core to provide an output roll 12 driven by being pressed against the surface of the roller 11. The roller 11 has a peripheral speed of 185  
25 metres per minute and thus there is a difference ratio of 1:0.85 between the peripheral speed of the third stretch roller 8 and that of the wind up roller 12 which is sufficient to allow substantial relaxation of the film before it is wound up. Thus, the plastics film from the  
30 feed roller 1 is subjected to a total stretch of 1:3.3 followed by a relaxation of 1:0.85 leading to a total stretch ratio of 1:2.85. The typical thickness of the stretched output material is 6.8, 8 or 9  $\mu\text{m}$ .